August 1, 2016

Mr. Andrew Fan, PE
US EPA Region III, 3LC20
1650 Arch Street
Philadelphia, PA 19103-2029

Ms. Barbara Brown
Project Coordinator
Maryland Department of the Environment
1800 Washington Blvd.
Baltimore, MD 21230

Re: ***COKE OVEN AREA INTERIM MEASURES PROGRESS REPORT 2ND QUARTER 2016***

Dear Mr. Fan and Ms. Brown:

On behalf of Tradepoint Atlantic and Sparrows Point, LLC, enclosed please find the Coke Oven Area Interim Measures Progress Report for the second quarter of 2016 completed for the Tradepoint Atlantic site. This report was distributed electronically on May 2, 2016 in accordance with the reporting requirements outlined in the US EPA Interim Measures Progress Report frequency letter dated March 26, 2013. Please advise if paper copies are required for your use and we will distribute accordingly.

The report summarizes implementation progress for the interim measures (IMs) that have been developed to address identified environmental conditions at the Coke Oven Area through June 30, 2016. Please contact me at (314) 620-3056 should questions arise during your review of the enclosed progress report.

Sincerely,

James Calenda

James Calenda
Project Manager

Enclosure

Introduction

This document presents operational data and monitoring information collected in the 2nd quarter of 2016 for Interim Measures (IMs) that have been installed to address identified environmental conditions at the former Coke Oven Area (COA) Special Study Area at the Sparrows Point Terminal site located in Sparrows Point, Maryland. This progress report summarizes IM performance including data collected from the 2nd quarter of 2016 and is submitted in accordance with reporting requirements outlined in correspondence received from US EPA on March 26, 2013. The following designations are applied in this document to identify the operating IM "Cells" (**Figure 1**) at the COA:

- Cell 1: Air Sparge/Soil Vapor Extraction (AS/SVE) System in the Former Benzol Processing Area,
- Cell 2: Air Sparge/Soil Vapor Extraction (AS/SVE) System in the shallow groundwater zone, groundwater pump and treat (GW P&T) system in the intermediate zone, Former Coal Basin Area,
- Cell 3: AS/SVE System in "Cove" Area,
- Cell 5: Dual Phase Extraction (DPE) system for the shallow zone, "Turning Basin" side of former Coke Oven Area,
- Cell 5: Dense Non-Aqueous Phase Liquid (DNAPL) Recovery
- Cell 6: Light Non-Aqueous Phase Liquid (LNAPL) Recovery at the Former Benzol Processing Area.

As of the end of the second quarter 2016, Cells 1, 2, 3, 5 and 6 remediation systems are operational.

Groundwater and soil gas sampling were conducted during the second quarter of 2016 to assess current conditions and removal efficiencies of the operating IM systems. The results of these sampling events, including trending graphs from IM startup, are detailed in this report. LNAPL removal continued at Cell 6 and DNAPL removal continued at Cell 5 without interruption. Additional detail on the design, operation and groundwater monitoring for these systems is provided in this progress report.

Cell 1: Prototype AS/SVE System in the Former Benzol Processing Area

Cell 1 consists of an AS/SVE system installed to remove volatile hydrocarbons that is coupled with vapor destruction via an electric catalytic oxidation (CATOX) unit. **Figure 2** shows the system layout of Cell 1 and locations of the major design components including the air sparging wells, vapor collection trenches and groundwater monitoring wells.

2nd Quarter 2016 Operational Performance

The system at Cell 1 underwent reconstruction to the air sparge piping and area layout. Construction was completed beginning of March during the 1st quarter of 2016. Once operations resumed, the air sparge system's performance was assessed to determine its most effective production settings. The sparge and vapor extraction operated continuously throughout the month of March during the 1st quarter 2016. During the 2nd quarter 2016 based on vapor recovery data, the decision was made to return to operating on a pulsing schedule; where the system is in recovery or on mode for one day and then turned off to let the area rebound for two or three days. This practice was implemented during the first quarter 2013 to improve recovery of hydrocarbons from the subsurface. Operations will continue to be in conformance with the manufacturer's specifications at all times that soil gases were collected in accordance with the May 20, 2011 modified permit-to-construct conditions as reflected in the Permit to Operate issued to Sparrows Point LLC on December 8, 2014.

Cell 1 experienced down-time due to necessary system repairs from May 21st to June 23rd during the second quarter of 2016. The VFD (variable frequency drive) controlling the SVE vacuum motor failed and the system was inoperable during that period. A new VFD has since been installed and Cell 1 returned to normal operation June 24th.

The hydrocarbon removal rate was calculated to be approximately 0.04 pounds per operating hour (estimated quarterly total of 49.8 pounds). **Table 1** also includes a cumulative summary of operational performance since system startup in August 3, 2010. In total, the AS/SVE system at Cell 1 has destroyed approximately 12,574 pounds of recovered hydrocarbons as shown graphically in **Figure 3**.

Soil gas sample collection occurred during the 2nd quarter of 2016 for laboratory analysis to monitor CATOX unit performance. One untreated soil gas sample for each month were collected in a Suma Canister during the 2nd quarter of 2016 and submitted to Pace Analytical Services, Inc. in Melville, New York for analysis by US EPA Method TO-15.

2nd Quarter 2016 Groundwater Monitoring Results

Groundwater samples were collected on June 23, 2016 from the following wells; the location of the wells are shown on Figure 2:

- CO93-PZM (former BP-MW-09 , upgradient of Cell 1),
- CO18-PZM006 (upgradient of Cell 1 at edge of berm), and
- CO02-PZM006 (downgradient of Cell 1).

The groundwater samples were submitted to Pace Analytical Services, Inc., located in Greensburg, Pennsylvania for the analyses shown in **Table 3**. These data indicate benzene is the most prevalent volatile organic compound (VOC) constituent. Since system startup in August 2010, a decreasing total VOC concentration trend is documented at the wells monitored for system performance as illustrated in **Figure 4**.

A recent increase in VOC concentration was observed in the 4th quarter 2015 and the 1st quarter 2016 data in the Cell 1 monitoring wells. This increase in total VOCs occurred during the restructuring of the cell 1 remediation system and is likely the cause of the recent increase. Monitoring wells CO02-PZM006 and CO18-PZM006 have shown a decrease in concentrations since the system returned to service, but monitoring well CO93-PZM displayed an increase in total VOC concentration as indicated in **Figure 4**. The analytical data for CO93-PZM will be reviewed and compared to future third quarter data to determine a trend. All other historical trending data for these monitoring wells will continue to be assessed during system operation in future months.

Cell 2: Air Sparge/Soil Vapor Extraction (AS/SVE) System in the Shallow Groundwater Zone, Groundwater Pump and Treat (GW P&T) System in the Intermediate Groundwater Zone, Former Coal Basin Area

Cell 2 consists of an AS/SVE system coupled with vapor destruction via an electric catalytic oxidation (CATOX) unit for volatile hydrocarbon groundwater treatment in the shallow zone and a pump and treat system for recovery of groundwater and volatile hydrocarbon treatment from the intermediate zone. The system design plans were approved by US EPA in correspondence received on September 10, 2013 and began full scale operation in October 2014. **Figure 5** shows the system layout of Cell 2 and locations of the major design components including the air sparging wells, vapor collection trenches, intermediate groundwater recovery wells, groundwater injection wells and groundwater monitoring well locations.

AS/SVE System

The delivery and recovery systems for the shallow AS/SVE system include the use of air sparge points and a horizontal vapor extraction trench. Eight (8) air sparge points along a 500 feet long stretch were installed near the shore line of Cell 2. Details of the air sparge zone and recovery trench include the following:

- Air sparge zone: 8 – 2-inch diameter AS points @ approximately 56 ft spacing, center to center (C-C)
    - Installed to 15 ft -17 ft bgs (bottom of slag fill)
    - Bottom 2 ft of each point to be screened with 20-slot screen

- Recovery trench
    - 500 ft of horizontal, 4-inch diameter perforated pipe (or 20-slot screen) installed to a total depth (TD) of 5 ft
    - 5 vertical 4-inch risers spaced every 100 ft, C-C
    - Top 2 ft is a clay cap
    - Geotextile fabric @ 2 ft bgs (under clay)
    - Granular screened slag backfill from 2 ft -5 ft
    - Horizontal recover piping located approximately 3 ft bgs (above water table)

GW P&T System

The pump and treat groundwater system includes a low profile air stripper that then utilizes an oxidizer to destroy all VOC vapors generated prior to exhausting to the atmosphere. The design groundwater flow is for a maximum of 40 gallons per minute (gpm). The oxidizer is sized to handle up to a 600 cubic feet per minute air flow. The recovery and re-injection systems include the use

of six groundwater recovery wells and six groundwater injection wells. The six recovery wells are installed along a 500 feet long stretch near the shore line of Cell 2.

- 6 – 4-inch diameter GW RWs @ approximately 83 ft spacing, C-C
  - Installed to 40-45 ft bgs (intermediate sand zone)
  - Bottom 15 ft of each RW screened with 20-slot screen
  - An electric pump in each RW, resting approximately 7-10 ft above the bottom of the well

- Recovered GW Treatment
  - Enters low profile air stripper
  - Off-gas sent to Electric Oxidizer for destruction
  - Treated groundwater pumped to six-6 inch diameter re-injection wells screened from 5 to 15 feet in depth for recirculation in shallow GW zone

2nd Quarter 2016 Operational Performance

AS/SVE System

Operational performance of the AS/SVE System at Cell 2 during this reporting period is summarized in **Table 4**. In summary, the CATOX unit operated for 1,440 hours (66%) during this reporting period. During 2nd quarter 2016, SVE operations were continuous. The system at Cell 2 was operated on a pulsing schedule during the 2nd quarter 2016 reporting quarter. Operations were in conformance with the manufacturer's specifications at all times that soil gases were collected in accordance with the March 24, 2014 permit-to-construct conditions as reflected in the Permit to Operate issued to Sparrows Point LLC on December 8, 2014.

The hydrocarbon removal rate was calculated to be approximately 0.003 pounds per operating hour (estimated quarterly total of 0.16 pounds). **Table 4** also includes a cumulative summary of operational performance since system startup in October 2014. In total, the AS/SVE system at Cell 2 has destroyed approximately 280.80 pounds of recovered hydrocarbons as shown graphically in **Figure 3**.

Soil gas samples were collected for laboratory analysis to monitor CATOX unit performance. One untreated soil gas sample per month is gathered each quarter. The samples were collected in a Suma Canister and submitted to Pace Analytical Services, Inc. in Melville, New York for analysis by US EPA Method TO-15. The average influent soil gas hydrocarbon concentration was 203 ug/m^3 as summarized in **Table 5**. Hydrocarbon removal calculations were based on the analytical results and the average daily field-measured influent flow rates. The mass removal calculations assume that the samples collected throughout the second quarter are representative of hydrocarbon concentrations for the entire quarter. This assumption is based on the fact that the same air sparge wells and extraction wells were online when the system was operational.

GW P&T System Evaluation

The Cell 2 groundwater pump and treat system was evaluated in the 2nd quarter 2016 with regard to the effectiveness of this system with respect to the mass of volatile hydrocarbons removed from groundwater.

Evaluation of Pump and Treat System Effectiveness

A total of 947,374 gallons of water were extracted from the Cell 2 Area pumping wells and treated during the 2nd quarter of 2016. The average pumping rate for the pump and treat system was 10,526 gpd, or 7.3 gpm.

Operations were in conformance with the manufacturer's specifications at all times that stripped hydrocarbons were discharged through the CaTOX unit to the atmosphere in accordance with the March 24, 2014 permit-to-construct conditions as reflected in the Permit to Operate issued to Sparrows Point LLC on December 8, 2014. In addition, treated groundwater discharges were in compliance with discharge permit conditions outlined in Discharge Permit 11-DP-3746 issued to Sparrows Point LLC on May 6, 2013. These pumping rates appear to effectively capture the most impacted groundwater beneath Cell 2, as revealed by **Figure 7** discussed in the following section.

A total of 416 lbs of benzene, toluene and xylene compounds (btex) and 17.7 lbs of naphthalene were removed and treated during the 2nd quarter of 2016. This total is shown graphically in **Figure 3**. The following table presents data for influent and effluent (treated) groundwater.

Field ID	Analysis	Units	13-JAN	28-JAN	4-FEB	22- FEB	21-MAR	22-MAR	**Quarter Average**
GWPT Cell 2 INFLUENT	Benzene	ug/L	31,000	28,000	48,000	51,000	58,000	65,000	**46,833**
GWPT Cell 2 INFLUENT	Toluene	ug/L	3000	2500	3800	3900	5800	7200	**4,367**
GWPT Cell 2 INFLUENT	Ethylbenzene	ug/L	0	0	0	0	270	360	**105**
GWPT Cell 2 INFLUENT	Total Xylenes	ug/L	700	570	820	890	2100	3390	**1,412**
GWPT Cell 2 INFLUENT	Naphthalene	ug/L	3800	1300	1500	970	4300	2100	**2,328**
GWPT Cell 2 EFFLUENT	Benzene	ug/L	230	220	140	0	230	55	**146**
GWPT Cell 2 EFFLUENT	Toluene	ug/L	23	24	13	0	18	5	**14**
GWPT Cell 2 EFFLUENT	Total Xylenes	ug/L	7	7	0	0	7	0	**4**
GWPT Cell 2 EFFLUENT	Naphthalene	ug/L	100	120	85	0	140	67	**85**

The pump and treat system is removing significant amounts of volatile hydrocarbons from groundwater within the intermediate water bearing zone at the current pumping rates, and it is controlling groundwater flow and associated migration within the intermediate water bearing zone.

2nd Quarter 2016 Groundwater Monitoring Results

Groundwater samples were collected in June 2016 from the following wells; the well locations are shown on **Figure 5**.

- CO27- PZM012 – shallow zone
- CO27-PZM046 - intermediate zone
- CO36-PZM008 – shallow zone
- CO36-PZM043 – intermediate zone
- CO37-PZM038 – intermediate zone
- CO38-PZM006 – shallow zone
- CO38-PZM043– intermediate zone
- CO39-PZM007– shallow zone
- CO39-PZM042– intermediate zone
- CO40-PZM008– shallow zone
- CO41-PZM 001– shallow zone
- CO41-PZM 036– intermediate zone
- CO42-PZM004 – shallow zone

Exception to the wells list as sampled in June is well CO37-PZM003. CO37-PZM003 was not sampled due to the presence of free product first identified in November 2014.

The groundwater samples were submitted to Pace Analytical Services, Inc., located in Greensburg, Pennsylvania for the analyses shown in **Table 7**. These data indicate benzene is the most prevalent volatile organic compound (VOC) constituent. The VOC concentrations for the 2nd quarter 2016 sampling events are shown for the groundwater wells monitored for system performance in **Figure 6A** and **6B**.

Shallow zone groundwater, with the exception of groundwater monitored at CO41-PZM001, has remained at consistent VOC levels since the first sampling event in 3rd quarter 2014. CO41-PZM001 had a significant increase of benzene during the 2nd quarter 2015 sampling event and had shown a steady decrease in concentrations throughout 3rd and 4th quarter 2015 sampling events. The increase of benzene found in CO41-PZM001 from 1st quarter 2016 sampling data has subsided to previous lower concentration levels from the 2nd quarter data. It may be determined that the groundwater treatment system has had the greatest effect within the subsurface area of the CO41-PZM001 MW location as data from this well reflects system

operation. No other significant increases or decreases in historical trends were present within the shallow zone.

Figure 7 presents a plan view of the concentration of VOCs in the intermediate zone from analytical results from the June 2016 monitoring event. No significant Increases or decreases were noted from the 2nd quarter 2016 groundwater data. These wells will continue to be monitored to assess possible trends associated with operation of the interim measure.

Light non-aqueous product (LNAPL) was encountered in well CO37-PZM003 in the shallow groundwater zone in November 2014. The well was hand baled multiple times recovering approximately 10 gallons of free product. The LNAPL levels were reduced and CO37-PZM003 was then hand baled on a monthly basis. The product level in CO37-PZM003 became trace during the last 2 quarters of 2015. It was then measured for product on a bi-weekly basis throughout the first and second quarters of 2016. For the second consecutive quarter, no product has shown a presence within the monitoring well. CO37-PZM003 will be sampled during the 3rd quarter sampling event.

Cell 3: AS/SVE System in the "Cove" Area

Cell 3 consists of an AS/SVE system coupled with vapor destruction via an electric CATOX unit. **Figure 1** shows the location of the Cell 3 AS/SVE treatment area at the COA. The major design components are described in the Cell 3 final design report (*Coke Oven Area Interim Measures Cell 3 "Cove" Area Air Sparge/Soil Vapor Extraction System Design*), submitted to US EPA on March 1, 2011.

2nd Quarter 2016 Operational Performance

Operational performance of Cell 3 during this reporting period is summarized in **Table 8**. In summary, the CATOX unit operated for 744 hours (34.1%) during the 2nd quarter of 2016. The system at Cell 3 continues to operate on a pulsing schedule; where the system is in recovery or on mode for one day and then turned off to let the area rebound for two or three days. This practice was implemented to improve recovery of hydrocarbons from the subsurface. Operations continue to be in conformance with the manufacturer's specifications at all times that soil gases were collected in accordance with the May 20, 2011 modified permit-to-construct conditions.

The hydrocarbon removal rate was calculated to be approximately 0.025 pounds per operating hour (estimated quarterly total of 18.866 pounds). **Table 8** also includes a cumulative summary of operational performance since system startup on June 24, 2011. In total, Cell 3 has destroyed approximately 1,680 pounds of recovered hydrocarbons as shown graphically in **Figure 3**.

Soil gas samples were collected for laboratory analysis to monitor CATOX unit performance. One untreated soil gas sample was collected in a Suma Canister and submitted to Pace Analytical Services. The average influent soil gas hydrocarbon concentration of the three samples taken throughout the 2nd quarter was 48,359 ug/m^3 as summarized in **Table 9**.

Hydrocarbon removal calculations were based entirely on the analytical results and the average daily field-measured influent flow rates. The mass removal calculations assume that the samples collected throughout the 2nd quarter are representative of hydrocarbon concentrations for the entire quarter. This assumption is based on the fact that the same air sparge wells (AS-2 thru AS-12) and extraction wells (V-2 thru V-4) were online when the system was operational. Operations at this Cell will continue to be evaluated in the future to improve system recovery rates.

2nd Quarter 2016 Groundwater Monitoring

Groundwater samples were collected in June 2016 from the following wells (**Figure 8**):

- CO101-PZM (downgradient of Cell 3),
- CO102-PZM (upgradient of Cell 3),
- CO103-PZM (upgradient of Cell 3),
- CO104-PZM (downgradient of cell 3),
- CO30-PZM015 (downgradient of Cell 3).

The groundwater samples were submitted to Pace Analytical for the analyses shown in **Table 10**. These data indicate that benzene is the most prevalent VOC constituent. Since system startup on June 24, 2011, a generally inconclusive VOC concentration trend is documented, as illustrated in **Figure 9**. Results from the last 4 quarters for CO103-PZM closely reflect historical concentrations for this well; therefore, it is interpreted that an increasing trend is not apparent in this well as potentially defined in the 3rd quarter of 2014. There were no increases or decreases of significance to any of the groundwater monitoring wells for the 2nd quarter of 2016. Groundwater will continue to be monitored and assessed during system operation in future months. The wells have shown relatively consistent concentrations over the last 2 years.

Cell 5: Dual Phase Extraction (DPE) System for the Shallow Zone, "Turning Basin" side of Former Coke Oven Area

Cell 5 consists of a dual phase (vapor and water) system (DPE) with a low profile air stripper followed by vapor phase granular activated carbon (VGAC) for removal and treatment of vapor and dissolved volatile hydrocarbons in the shallow groundwater zone. The system design plans were approved by US EPA in correspondence received on September 10, 2013 and began full scale operation in October 2014. **Figure 10** shows the system layout of Cell 5 and locations of the major design components including the dual phase recovery points, treatment system, groundwater injection wells and groundwater monitoring well locations.

The recovery and re-injection systems include the use of dual phase (soil vapor and groundwater) recovery wells and six groundwater re-injection wells. Twelve (12) recovery wells were installed along an approximate 500 feet long stretch downgradient of the most recent 10,000 ug/L is contour line for naphthalene (between the naphthalene source area and the eastern shore line along the Turning Basin).

- 12 – 1.5-inch diameter DPE RWs @ approximately 42 ft spacing, C-C
  - Installed to 15-17 ft bgs (to bottom of shallow slag)
  - Bottom 2 ft of each RW screened with 20-slot screen
  - Vapor recovery perforations located between 10-12 ft bgs

- Recovered GW and vapor Treatment
  - Enters MS knockout tank to separate air and water phases
  - Water sent to low profile air stripper
  - Off-gas sent to VGAC for capture
  - Treated groundwater pumped to six-6 inch diameter re-injection wells screened from 5 to 15 feet in depth for recirculation in shallow GW zone

2nd Quarter 2016 Operational Performance

Evaluation of Pump and Treat System Effectiveness

A total of 1,407,139 gallons of water were extracted from the Cell 5 Area dual phase extraction wells and treated during the 2nd quarter of 2016. The average recovery rate for the DPE system was 15,634 gpd (10.8 gpm).

Operations were in conformance with the manufacturer's specifications at all times that stripped hydrocarbons were discharged to the atmosphere in accordance with the March 24,

2014 permit-to-construct conditions as reflected in the Permit to Operate issued to Sparrows Point LLC on December 8, 2014.

A total of 12 pounds (lbs) of benzene, toluene and xylene compounds (btex) and 58 pounds (lbs) of naphthalene were removed during the 2nd quarter of 2016. This total is shown graphically in **Figure 3**. The following table presents data for influent and effluent (treated) groundwater.

Field ID	Analysis	Units	18-Apr	19-Apr	27-May	31-May	17-Jun	20-Jun	**AVG**
GWPT Cell 5 INFLUENT	Benzene	ug/L	520	490	360	0	330	550	375
GWPT Cell 5 INFLUENT	Toluene	ug/L	330	310	210	0	180	280	218
GWPT Cell 5 INFLUENT	Styrene	ug/L	110	100	69	0	72	96	74.5
GWPT Cell 5 INFLUENT	Total Xylenes	ug/L	490	460	307	0	280	430	328
GWPT Cell 5 INFLUENT	Naphthalene	ug/L	5300	5300	3700	800	7300	7,300	4,950
GWPT Cell 5 EFFLUENT	Benzene	ug/L	0	0	0	0	0	0	0
GWPT Cell 5 EFFLUENT	Toluene	ug/L	0	0	0	0	0	0	0
GWPT Cell 5 EFFLUENT	Total Xylenes	ug/L	0	0	0	0	0	0	0
GWPT Cell 5 EFFLUENT	Naphthalene	ug/L	0	0	0	0	0	0	0

The DPE system is removing volatile hydrocarbons from groundwater within the shallow water bearing zone at the current recovery rates. The system has shown continual improvement in performance since the first few quarters of operation, mostly attributed to the recent addition of the liquid carbon treatment tanks during the 2nd quarter of 2015.

The Cell 5 groundwater treatment system experienced 2 weeks of down-time during the 2nd quarter of 2016 for MS tank repairs and eventual replacement. From 5/24 until 5/31, the cell 5 remediation system was stopped for repairs to the leaking MS tank. From 6/6 until

6/10, the system was stopped for the replacement of the MS tank. No other significant periods of down-time occurred with the system throughout the quarter.

2nd Quarter 2016 Groundwater Monitoring Results

Groundwater samples were collected in June 2016 from the following shallow zone monitoring wells; the well locations are shown on **Figure 10**.

- CO23- PZM008
- CO24-PZM007
- CO26-PZM007
- CO55-PZM000
- CO56-PZP001
- CO57-PZP002
- CO58-PZM001
- CO59-PZP002
- CO60-PZP001

The groundwater samples were submitted to Pace Analytical Services, Inc., located in Greensburg, Pennsylvania for the analyses shown in **Table 11**. These data indicate naphthalene is the most prevalent hydrocarbon constituent. The naphthalene concentrations for the 2014-2016 sampling events are shown for the groundwater wells monitored for system performance as illustrated in **Figure 11A** and **11B. Figure 14A** presents shallow groundwater naphthalene concentration trends for wells presumed to be upgradient of the treatment system. No apparent trends are present in the analytical data. This presumed upgradient set of wells will continue to be monitored to further assess possible trends associated with operation of the interim measure in future quarters.

CO26-PZM007 resides within the presumed downgradient group of monitoring wells. The groundwater analyzed from this well during the 1st quarter 2016 sampling event showed an increase in naphthalene concentration. The concentration has since decreased from 12,800 ug/L naphthalene in the 1st quarter data to 2,140 ug/L naphthalene in the 2nd quarter. The 1st quarter concentration increase may have been caused from downtime of the groundwater remediation system for cell 5 during that quarter. This monitoring well will continue to be monitored for trends in future sampling events. **Figure 12** presents a plan view of the concentration of naphthalene in the shallow zone from analytical results from the June 2016 monitoring event.

Cell 5: DNAPL Extraction

DNAPL product removal began to be extracted from the Cell 5 area in the latter part of the 4th quarter 2015. DNAPL was extracted from several newly constructed extraction wells that have constructed DNAPL sumps below the screened interval. Compressed air DNAPL skimmer pumps were installed within two specific extraction wells that had shown to produce the greatest amounts of DNAPL: CO123-PZM and CO125-PZM. A 55-gallon drum has been placed next to CO125-PZM and a 500-gallon holding tank was placed at CO123-PZM. Product that is removed from the wells is pumped into the holding containers and taken offsite every 90 days. **Table 12** summarizes 1) DNAPL occurrence and recovery observed in monitoring wells for this Cell during the reporting period, 2) the start date of extraction from recovery wells and 3) cumulative DNAPL recovered since the beginning of the interim measure.

The DNAPL was recovered from the following wells:

Well	**DNAPL Recovery (gal/lbs)**	
	2nd Qtr 2016 (gal/lbs)	**Total thru 2nd Qtr 2016 (gal/lbs)**
CO123-PZMxxx	53/509	198/1900
CO125-PZMxxx	0/0	100/960
Total	**53/509**	**298/2860**

Cell 6: LNAPL Extraction at the Former Benzol Processing Area

The Cell 6 LNAPL monitoring and recovery system was monitored weekly during the 2nd quarter of 2016. **Table 13** summarizes; 1) LNAPL occurrence and recovery observed in monitoring wells for this Cell during the reporting period, 2) the start date of extraction from recovery wells and 3) cumulative LNAPL recovered since the beginning of the interim measure. **Figure 13** illustrates the well locations. An estimated 770 gallons (5,643 pounds) of LNAPL were recovered during the 2nd quarter 2016, bringing the total recovered LNAPL to 15,398 gallons (112,837 pounds) as of July 6, 2016. Well BP-MW-10 did not produce measurable amounts of LNAPL. LNAPL was recovered from wells in the Cell 6 area as shown below. The LNAPL was recovered from the following wells:

Well	Previous Well Identifier	LNAPL Recovery (gal/lbs)	
		2nd Qtr 2016 (gal/lbs)	Total thru 2nd Qtr 2016 (gal/lbs)
CO99-PZMxxx	RW-04	124/909	1,822/13,352
CO89-PZMxxx	BP-MW-05	218/1,598	9,849/72,173
CO92-PZMxxx	BP-MW-08	63/462	1,851/13,564
CO95-PZMxxx	BP-MW-11	365/2,675	1,756/12,868
CO97-PZMxxx	RW-02	0/0	0.8/6
CO98-PZMxxx	RW-03	0/0	118/865
CO96-PZMxxx	RW-01	0/0	1.3/10
	TOTAL	**770/5,643**	**15,398/112,837**

Table 14 provides well-specific details concerning the measured depths to LNAPL, the water table, and calculated LNAPL thicknesses for monitoring wells in the Cell 6 area.

TABLES

Table 1
Summary of Operation Conditions
Cell 1: Prototype AS/SVE System in Former Benzol Processing Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Cell 1 Second Quarter 2016 Estimated Hydrocarbon Recovery

Parameter	Units	Quantity
Total CATOX Operating Time (April 1, 2016 - June 30, 2016)	hours	1,128
Overall CATOX Operational Time	%	52.2%
Estimated Total Hydrocarbons Destroyed	pounds	49.829
Estimated Hydrocarbon Removal Rate	pounds/hour	0.04417

Cell 1 Cumulative Summary of Estimated Hydrocarbon Recovery

Parameter	Units	Quantity
Total ICE/CATOX Operating Time (August 3, 2010 - June 30, 2016)	hours	24,220
Overall CATOX Operational Time	%	55.5%
Estimated Total Hydrocarbons Destroyed	pounds	12,574
Estimated Hydrocarbon Removal Rate	pounds/hour	0.52

Table 2
Summary of Soil Gas Analytical Results (Second Quarter 2016)
Cell 1: Prototype AS/SVE System in Former Benzol Processing Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Analyte	Sample ID Date Time Dilution Factor Units	CATOX Influent Q2 2016
TO-15 Volatile Organics		
Acetone	ug/m^3	**21**
Benzene	ug/m^3	**64,700**
Bromoform	ug/m^3	ND
2-Butanone (MEK)	ug/m^3	ND
Carbon disulfide	ug/m^3	**0**
Carbon tetrachloride	ug/m^3	ND
Chlorobenzene	ug/m^3	ND
Chloroethane	ug/m^3	**1**
Chloroform	ug/m^3	ND
1,1-Dichloroethane	ug/m^3	ND
1,2-Dichloroethane	ug/m^3	ND
1,1-Dichloroethene	ug/m^3	ND
trans-1,2-Dichloroethene	ug/m^3	ND
1,2-Dichloropropane	ug/m^3	ND
cis-1,3-Dichloropropene	ug/m^3	ND
trans-1,3-Dichloropropene	ug/m^3	ND
Ethylbenzene	ug/m^3	**1,052**
2-Hexanone	ug/m^3	ND
Methylene Chloride	ug/m^3	**4**
4-Methyl-2-pentanone (MIBK)	ug/m^3	ND
1,1,2,2-Tetrachloroethane	ug/m^3	ND
Tetrachloroethene	ug/m^3	**0**
Toluene	ug/m^3	**23,450**
1,1,1-Trichloroethane	ug/m^3	ND
1,1,2-Trichloroethane	ug/m^3	ND
Trichloroethene	ug/m^3	ND
Vinyl chloride	ug/m^3	ND
m&p-Xylene	ug/m^3	**8,840**
o-Xylene	ug/m^3	**3,595**
Total Volatile Organics	ug/m^3	**101,663**

Notes:

VOC concentrations are averages derived from the 3 monthly influent air samples taken during the quarter (one sample taken each month of the quarter)

BOLD = Analyte detected

ug/m^3 = micro grams per cubic meter

ND = Analyte not detected above laboratory reporting limit

Table 3
Summary of Groundwater Analytical Results (Second Quarter 2016)
Cell 1: Prototype AS/SVE System in Former Benzol Processing Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

New Sample ID		CO02-PZM006	CO18-PZM006	CO93-PZMxxx
Former Sample ID		CO02-PZM006	CO18-PZM006	BP-MW-09
Date		6/23/2016	6/23/2016	6/23/2016
Analyte	Units			
Volatile Organics				
1,1,1,2-Tetrachloroethane	µg/L	ND	ND	ND
1,1,1-Trichloroethane	µg/L	ND	ND	ND
1,1,2,2-Tetrachloroethane	µg/L	ND	ND	ND
1,1,2-Trichloroethane	µg/L	ND	ND	ND
1,1-Dichloroethane	µg/L	ND	ND	ND
1,1-Dichloroethene	µg/L	ND	ND	ND
1,2,3-Trichloropropane	µg/L	ND	ND	ND
1,2-Dibromo-3-chloropropane	µg/L	ND	ND	ND
1,2-Dibromoethane (EDB)	µg/L	ND	ND	ND
1,2-Dichlorobenzene	µg/L	ND	ND	ND
1,2-Dichloroethane	µg/L	ND	ND	ND
1,2-Dichloropropane	µg/L	ND	ND	ND
1,4-Dichlorobenzene	µg/L	ND	ND	ND
2-Butanone (MEK)	µg/L	ND	ND	ND
2-Hexanone	µg/L	ND	ND	ND
4-Methyl-2-pentanone (MIBK)	µg/L	ND	ND	ND
Acetone	µg/L	ND	ND	ND
Acrylonitrile	µg/L	ND	ND	ND
Benzene	µg/L	**205,000**	**227,000**	**507,000**
Bromochloromethane	µg/L	ND	ND	ND
Bromodichloromethane	µg/L	ND	ND	ND
Bromoform	µg/L	ND	ND	ND
Bromomethane	µg/L	ND	ND	ND
Carbon disulfide	µg/L	ND	ND	**38.2**
Carbon tetrachloride	µg/L	ND	ND	ND
Chlorobenzene	µg/L	ND	ND	**17.9**
Chloroethane	µg/L	ND	ND	ND
Chloroform	µg/L	ND	ND	ND
Chloromethane	µg/L	ND	ND	ND
Dibromochloromethane	µg/L	ND	ND	ND
Dibromomethane	µg/L	ND	ND	ND
Ethylbenzene	µg/L	**451**	**57**	**1,860**
Iodomethane	µg/L	ND	ND	ND
Methyl-tert-butyl ether	µg/L	ND	ND	ND
Methylene Chloride	µg/L	ND	ND	ND
Styrene	µg/L	**8.5**	**ND**	**1,840**
Tetrachloroethene	µg/L	ND	ND	ND
Toluene	µg/L	**2,500**	**3,700**	**62,700**
Trichloroethene	µg/L	ND	ND	ND
Trichlorofluoromethane	µg/L	ND	ND	ND
Vinyl acetate	µg/L	ND	ND	ND
Vinyl chloride	µg/L	ND	ND	ND
Xylene (Total)	µg/L	**1,590**	**1,130**	**25,000**
cis-1,2-Dichloroethene	µg/L	ND	ND	ND
cis-1,3-Dichloropropene	µg/L	ND	ND	ND
trans-1,2-Dichloroethene	µg/L	ND	ND	ND
trans-1,3-Dichloropropene	µg/L	ND	ND	ND
trans-1,4-Dichloro-2-butene	µg/L	ND	ND	ND
Total Volatile Organics	µg/L	**209,550**	**231,887**	**598,456**
Semi-Volatiles				
Naphthalene	µg/L	**392**	**132**	**11,900**

Notes:

Bold = Analyte Detected

ND = Analyte not detected above laboratory reporting limit

µg/L = Micrograms per liter

Table 4
Summary of Operation Conditions
Cell 2 AS/SVE System
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Cell 2 Second Quarter 2016 Estimated Hydrocarbon Recovery

Parameter	Units	Quantity
Total CATOX Operating Time (April 1, 2016 - June 30, 2016)	hours	1,440
Overall CATOX Operational Time	%	65.9%
Estimated Total Hydrocarbons Destroyed	pounds	0.16
Estimated Hydrocarbon Removal Rate	pounds/hour	0.0001

Cell 2 Cumulative Summary of Estimated Hydrocarbon Recovery

Parameter	Units	Quantity
Total ICE/CATOX Operating Time (October 1, 2014 - March 31, 2016)	hours	10,032
Overall CATOX Operational Time	%	65.5%
Estimated Total Hydrocarbons Destroyed	pounds	280.80
Estimated Hydrocarbon Removal Rate	pounds/hour	0.028

Table 5
Summary of Soil Gas Analytical Results (Second Quarter 2016)
Cell 2 AS/SVE System
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Analyte	Sample ID Date Time Dilution Factor Units	CATOX Influent Q2 2016
TO-15 Volatile Organics		
Acetone	ug/m^3	ND
Benzene	ug/m^3	**90**
Bromoform	ug/m^3	ND
2-Butanone (MEK)	ug/m^3	ND
Carbon disulfide	ug/m^3	ND
Carbon tetrachloride	ug/m^3	**2**
Chlorobenzene	ug/m^3	ND
Chloroethane	ug/m^3	ND
Chloroform	ug/m^3	ND
1,1-Dichloroethane	ug/m^3	ND
1,2-Dichloroethane	ug/m^3	ND
1,1-Dichloroethene	ug/m^3	ND
trans-1,2-Dichloroethene	ug/m^3	ND
1,2-Dichloropropane	ug/m^3	ND
cis-1,3-Dichloropropene	ug/m^3	ND
trans-1,3-Dichloropropene	ug/m^3	ND
Ethylbenzene	ug/m^3	**4**
2-Hexanone	ug/m^3	ND
Methylene Chloride	ug/m^3	**10**
4-Methyl-2-pentanone (MIBK)	ug/m^3	ND
1,1,2,2-Tetrachloroethane	ug/m^3	ND
Tetrachloroethene	ug/m^3	ND
Toluene	ug/m^3	**62**
1,1,1-Trichloroethane	ug/m^3	ND
1,1,2-Trichloroethane	ug/m^3	ND
Trichloroethene	ug/m^3	ND
Vinyl chloride	ug/m^3	ND
m&p-Xylene	ug/m^3	**19**
o-Xylene	ug/m^3	**15**
Total Volatile Organics	ug/m^3	**203**

Notes:

VOC concentrations are averages derived from the 3 monthly influent air samples taken during the quarter (one sample taken each month of the quarter)

BOLD = Analyte detected

ug/m^3 = micro grams per cubic meter

ND = Analyte not detected above laboratory reporting limit

Table 7
Summary of Groundwater Analytical Results (Second Quarter 2016)
Cell 2
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

New Sample ID		CO27-PZM012	CO27-PZM046	CO36-PZM008	CO36-PZM043	CO37-PZM038	CO37-PZM003	CO38-PZM043	CO38-PZM006	CO39-PZM007	CO39-PZM042	CO40-PZM008	CO41-PZM001	CO41-PZM036	CO42-PZM004
Former Sample ID		CO27-PZM012	CO27-PZM046	Cell 2-MW1 (S)	Cell2-MW8 (I)	Cell2-MW9 (I)	Cell2-MW2 (S)	Cell2-MW10 (I)	Cell2-MW3 (S)	Cell2-MW4 (S)	Cell2-MW11 (I)	Cell2-MW5 (S)	Cell2-MW6 (S)	Cell2-MW12 (I)	Cell2-MW7 (S)
Date		6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016	6/22/2016
Analyte	Units														
Volatile Organics															
1,1,1,2-Tetrachloroethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,1,1-Trichloroethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,1,2,2-Tetrachloroethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,1,2-Trichloroethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,1-Dichloroethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,1-Dichloroethene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,2,3-Trichloropropane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dibromo-3-chloropropane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dibromoethane (EDB)	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichloroethane	µg/L	ND	ND	ND	**799**	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichloropropane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
2-Butanone (MEK)	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
2-Hexanone	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
4-Methyl-2-pentanone (MIBK)	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Acetone	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Acrylonitrile	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Benzene	µg/L	**19,400**	**436,000**	**22,300**	**25,400**	**22,900**	NS	**9**	**9,350**	**8,760**	**29,300**	**292**	**5,170**	**291,000**	**661**
Bromochloromethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Bromodichloromethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Bromoform	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Bromomethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Carbon disulfide	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Carbon tetrachloride	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Chlorobenzene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	**ND**	ND
Chloroethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Chloroform	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Chloromethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Dibromochloromethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Dibromomethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Ethylbenzene	µg/L	**177**	**979**	**59.9**	**71.6**	**322**	NS	ND	**104**	**41.2**	**276**	**4.4**	**67**	**1,200**	**176**
Iodomethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Methyl-tert-butyl ether	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Methylene Chloride	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Styrene	µg/L	**215**	**238**	**19.1**	**18.6**	**540**	NS	ND	**49.4**	**51.4**	**464**	**ND**	**3.3**	**474**	**89.9**
Tetrachloroethene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Toluene	µg/L	**7,000**	**70,000**	**4,880**	**4,020**	**11,900**	NS	ND	**1,970**	**1,980.0**	**12,600**	**123**	**3,170**	**116,000**	**1,700**
Trichloroethene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Trichlorofluoromethane	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Vinyl acetate	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Vinyl chloride	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Xylene (Total)	µg/L	**1,610**	**18,200**	**1,210**	**1,040**	**2,620**	NS	ND	**722**	**357.0**	**2,430**	**69.5**	**864**	**26,000**	**1,930**
cis-1,2-Dichloroethene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
cis-1,3-Dichloropropene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
trans-1,2-Dichloroethene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
trans-1,3-Dichloropropene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
trans-1,4-Dichloro-2-butene	µg/L	ND	ND	ND	ND	ND	NS	ND	ND	ND	ND	ND	ND	ND	ND
Total Volatile Organics	µg/L	**28,402**	**525,417**	**28,469**	**31,349**	**38,282**	**0**	**9**	**12,195**	**11,190**	**45,070**	**489**	**9,274**	**434,674**	**4,557**
Semi-Volatiles															
Naphthalene	µg/L	**756**	**13,700**	**382**	**562**	**14,000**	NS	**0**	**780**	**1,570**	**7,680**	**376**	**66.6**	**190**	**3,650**

Notes:

Bold = Analyte Detected

ND = Analyte not detected above laboratory reporting limit

µg/L = Micrograms per liter

Table 8
Summary of Operation Conditions
Cell 3: AS/SVE System in the "Cove" Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Cell 3 Second Quarter 2016 Estimated Hydrocarbon Recovery

Parameter	Units	Quantity
Total CATOX Operating Time (April 1, 2016 - June 30, 2016)	hours	744
Overall CATOX Operational Time	%	34.1%
Estimated Total Hydrocarbons Destroyed	pounds	18.866
Estimated Hydrocarbon Removal Rate	pounds/hour	0.025357

Cell 3 Cumulative Summary of Estimated Hydrocarbon Recovery

Parameter	Units	Quantity
Total ICE/CATOX Operating Time (August 3, 2010 - June 30, 2016)	hours	18,959
Overall CATOX Operational Time	%	59.0%
Estimated Total Hydrocarbons Destroyed	pounds	1,680.4
Estimated Hydrocarbon Removal Rate	pounds/hour	0.09

Table 9
Summary of Soil Gas Analytical Results (Second Quarter 2016)
Cell 3: AS/SVE System in the "Cove" Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Analyte	Sample ID Date Time Dilution Factor Units	CATOX Influent Q2 2016
TO-15 Volatile Organics		
Acetone	ug/m^3	**8,600**
Benzene	ug/m^3	**35,100**
Bromoform	ug/m^3	ND
2-Butanone (MEK)	ug/m^3	ND
Carbon disulfide	ug/m^3	ND
Carbon tetrachloride	ug/m^3	ND
Chlorobenzene	ug/m^3	ND
Chloroethane	ug/m^3	ND
Chloroform	ug/m^3	ND
1,1-Dichloroethane	ug/m^3	ND
1,2-Dichloroethane	ug/m^3	ND
1,1-Dichloroethene	ug/m^3	ND
trans-1,2-Dichloroethene	ug/m^3	ND
1,2-Dichloropropane	ug/m^3	ND
cis-1,3-Dichloropropene	ug/m^3	ND
trans-1,3-Dichloropropene	ug/m^3	ND
Ethylbenzene	ug/m^3	**55**
2-Hexanone	ug/m^3	ND
Methylene Chloride	ug/m^3	ND
4-Methyl-2-pentanone (MIBK)	ug/m^3	ND
1,1,2,2-Tetrachloroethane	ug/m^3	ND
Tetrachloroethene	ug/m^3	ND
Toluene	ug/m^3	**3,553**
1,1,1-Trichloroethane	ug/m^3	ND
1,1,2-Trichloroethane	ug/m^3	ND
Trichloroethene	ug/m^3	ND
Vinyl chloride	ug/m^3	ND
m&p-Xylene	ug/m^3	**714**
o-Xylene	ug/m^3	**337**
Total Volatile Organics	ug/m^3	**48,359**

Notes:

VOC concentrations are averages derived from the 3 monthly influent air samples taken during the quarter (one sample taken each month of the quarter)

BOLD = Analyte detected

ug/m^3 = micro grams per cubic meter

ND = Analyte not detected above laboratory reporting limit

Table 10
Summary of Groundwater Analytical Results (Second Quarter 2016)
Cell 3: AS/SVE System in the "Cove" Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

New Sample ID		CO30-PZM015	CO101-PZM	CO102-PZM	CO103-PZM	CO104-PZM
Former Sample ID		CO30-PZM015	MW-CELL 3-1	MW-CELL 3-2	MW-CELL 3-3	MW-CELL 3-4
Date		6/23/2016	6/23/2016	6/23/2016	6/23/2016	6/23/2016
Analyte	Units					
Volatile Organics						
1,1,1,2-Tetrachloroethane	µg/L	ND	ND	ND	ND	ND
1,1,1-Trichloroethane	µg/L	ND	ND	ND	ND	ND
1,1,2,2-Tetrachloroethane	µg/L	ND	ND	ND	ND	ND
1,1,2-Trichloroethane	µg/L	ND	ND	ND	ND	ND
1,1-Dichloroethane	µg/L	ND	ND	ND	ND	ND
1,1-Dichloroethene	µg/L	ND	ND	ND	ND	ND
1,2,3-Trichloropropane	µg/L	ND	ND	ND	ND	ND
1,2-Dibromo-3-chloropropane	µg/L	ND	ND	ND	ND	ND
1,2-Dibromoethane (EDB)	µg/L	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	µg/L	ND	ND	ND	ND	ND
1,2-Dichloroethane	µg/L	ND	ND	ND	ND	ND
1,2-Dichloropropane	µg/L	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	µg/L	ND	ND	ND	ND	ND
2-Butanone (MEK)	µg/L	ND	ND	ND	ND	ND
2-Hexanone	µg/L	ND	ND	ND	ND	ND
4-Methyl-2-pentanone (MIBK)	µg/L	ND	ND	ND	ND	ND
Acetone	µg/L	ND	ND	ND	ND	ND
Acrylonitrile	µg/L	ND	ND	ND	ND	ND
Benzene	µg/L	**71,600**	**23,800**	**23,000**	**37,900**	**13.7**
Bromochloromethane	µg/L	ND	ND	ND	ND	ND
Bromodichloromethane	µg/L	ND	ND	ND	ND	ND
Bromoform	µg/L	ND	ND	ND	ND	ND
Bromomethane	µg/L	ND	ND	ND	ND	ND
Carbon disulfide	µg/L	ND	ND	ND	ND	ND
Carbon tetrachloride	µg/L	ND	ND	ND	ND	ND
Chlorobenzene	µg/L	ND	ND	ND	ND	ND
Chloroethane	µg/L	ND	ND	ND	ND	ND
Chloroform	µg/L	ND	ND	ND	ND	ND
Chloromethane	µg/L	ND	ND	ND	ND	ND
Dibromochloromethane	µg/L	ND	ND	ND	ND	ND
Dibromomethane	µg/L	ND	ND	ND	ND	ND
Ethylbenzene	µg/L	**101**	**31.8**	**33.7**	**78**	ND
Iodomethane	µg/L	ND	ND	ND	ND	ND
Methyl-tert-butyl ether	µg/L	ND	ND	ND	ND	ND
Methylene Chloride	µg/L	ND	ND	ND	ND	ND
Styrene	µg/L	**19.3**	**10.2**	**11.1**	**16.2**	ND
Tetrachloroethene	µg/L	ND	ND	ND	ND	ND
Toluene	µg/L	**4,850**	**1,630**	**851**	**3,190**	**1.4**
Trichloroethene	µg/L	ND	ND	ND	ND	ND
Trichlorofluoromethane	µg/L	ND	ND	ND	ND	ND
Vinyl acetate	µg/L	ND	ND	ND	ND	ND
Vinyl chloride	µg/L	ND	ND	ND	ND	ND
Xylene (Total)	µg/L	**1,440**	**368**	**372**	**1,330**	ND
cis-1,2-Dichloroethene	µg/L	ND	ND	ND	ND	ND
cis-1,3-Dichloropropene	µg/L	ND	ND	ND	ND	ND
trans-1,2-Dichloroethene	µg/L	ND	ND	ND	ND	ND
trans-1,3-Dichloropropene	µg/L	ND	ND	ND	ND	ND
trans-1,4-Dichloro-2-butene	µg/L	ND	ND	ND	ND	ND
Total Volatile Organics	µg/L	**78,010**	**25,840**	**24,268**	**42,514**	**15**
Semi-Volatiles						
Naphthalene	µg/L	**19,500**	**4,040**	**9,900**	**18,300**	**5.3**

Notes:

Bold = Analyte Detected

ND = Analyte not detected above laboratory reporting limit

µg/L = Micrograms per liter

Table 11
Summary of Groundwater Analytical Results (Second Quarter 2016)
Cell 5 DPE Groundwater Pump and Treat System
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

New Sample ID		CO23-PZM008	CO24-PZM007	CO26-PZM007	CO55-PZM000	CO56-PZP001	CO57-PZP002	CO58-PZM001	CO59-PZP002	CO60-PZP001
Former Sample ID		CO23-PZM008	CO24-PZM007	CO26-PZM007	Cell5-MW1 (S)	Cell5-MW2 (S)	Cell5-MW3 (S)	Cell5-MW4 (S)	Cell5-MW5 (S)	Cell5-MW6 (S)
Date		6/24/2016	6/24/2016	6/24/2016	6/24/2016	6/24/2016	6/24/2016	6/24/2016	6/24/2016	6/24/2016
Time										
Analyte	Units									
Volatile Organics										
1,1,1,2-Tetrachloroethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,1,1-Trichloroethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,1,2,2-Tetrachloroethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,1,2-Trichloroethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,1-Dichloroethane	µg/L	ND	ND	ND	ND	ND	ND	**0.46**	ND	ND
1,1-Dichloroethene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2,3-Trichloropropane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dibromo-3-chloropropane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dibromoethane (EDB)	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichlorobenzene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichloroethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,2-Dichloropropane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
1,4-Dichlorobenzene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
2-Butanone (MEK)	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
2-Hexanone	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
4-Methyl-2-pentanone (MIBK)	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Acetone	µg/L	ND	ND	ND	**36.1**	ND	**134**	ND	ND	ND
Acrylonitrile	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Benzene	µg/L	**636**	**5.3**	**365**	**8.2**	**380**	ND	**247**	**9.5**	**189**
Bromochloromethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Bromodichloromethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Bromoform	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Bromomethane	µg/L	ND	ND	**3.8**	ND	ND	**7.8**	ND	**4.2**	ND
Carbon disulfide	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Carbon tetrachloride	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Chlorobenzene	µg/L	ND	ND	**0.3**	ND	ND	ND	ND	ND	ND
Chloroethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Chloroform	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Chloromethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Dibromochloromethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Dibromomethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Ethylbenzene	µg/L	**31.6**	**5.5**	**16**	ND	**15.1**	ND	**13.8**	**0.6**	**6.1**
Iodomethane	µg/L	ND	ND	ND	ND	ND	ND	ND	**4.3**	ND
Methyl-tert-butyl ether	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Methylene Chloride	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Styrene	µg/L	**21.1**	ND	**83.7**	ND	**62**	ND	**36.7**	ND	**16.2**
Tetrachloroethene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Toluene	µg/L	**413**	**4.1**	**206**	**4.3**	**176**	ND	**93.2**	**4.7**	**25.8**
Trichloroethene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Trichlorofluoromethane	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Vinyl acetate	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Vinyl chloride	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Xylene (Total)	µg/L	**474**	**12.2**	**344**	**6**	**281**	ND	**218**	**7.4**	**123**
cis-1,2-Dichloroethene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
cis-1,3-Dichloropropene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
trans-1,2-Dichloroethene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
trans-1,3-Dichloropropene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
trans-1,4-Dichloro-2-butene	µg/L	ND	ND	ND	ND	ND	ND	ND	ND	ND
Semi-Volatiles										
Naphthalene	µg/L	**9,640**	**3,950**	**2,140**	**92.2**	**10,800**	**0.0**	**3,610**	**34.7**	**892**
Total Volatile Organics	µg/L	**11,216**	**3,977**	**3,159**	**147**	**11,714**	**142**	**4,219**	**65**	**1,252**

Notes:

Bold = Analyte Detected

ND = Analyte not detected above laboratory reporting limit

µg/L = Micrograms per liter

Table 12
DNAPL Occurrence and Recovery
Cell 5: DNAPL Recovery System
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Well ID	DNAPL Occurrence During Second Quarter 2016 (ft)	Total DNAPL Recovery Period		Cumulative Total DNAPL Recovered		Estimate DNAPL Recovered During Second Quarter 2016	
		Begin	End	(gal)	(lbs) (a)	(gal)	(lbs) (a)
CO123-PZMxxx	8.33	1-Jan-16	On-going (b)	198	1,900	53	509
CO125-PZMxxx	2.08	1-Jan-16	On-going (b)	100	960	0	0
CO124-PZMxxx	8.82	na	na	0	0	0	0
			Total Recovery:	**298**	**2,860**	**53**	**509**

Notes:

(a) Weight is calculated based on oil density of 1.15 grams per cubic centimeter.

(b) Skimmer

(c) Bailing

Table 13
LNAPL Occurrence and Recovery
Cell 6: LNAPL Recovery System in Former Benzol Processing Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Well ID	Former Well ID	LNAPL Occurrence During Second Quarter 2016 (ft)	Total LNAPL Recovery Period		Cumulative Total LNAPL Recovered		Estimate LNAPL Recovered During Second Quarter 2016	
			Begin	End	(gal)	(lbs) (a)	(gal)	(lbs) (a)
CO99-PZMxxx	RW-04	0.37	23-Jul-10	On-going (b)	1,818	13,322	120	879
CO89-PZMxxx	BP-MW-05	1.09	28-Jan-10	On-going (b)	9,832	72,049	201	1,473
CO92-PZMxxx	BP-MW-08	0.38	8-Sep-10	On-going (b)	1,851	13,564	63	462
CO95-PZMxxx	BP-MW-11	1.02	23-Jul-10	On-going (b)	2,176	15,946	360	2,638
CO97-PZMxxx	RW-02	0.04	28-Jan-11	On-going (c)	0.8	6	0	0
CO98-PZMxxx	RW-03	0.19	24-Nov-10	On-going (c)	118	865	0	0
CO96-PZMxxx	RW-01	0.19	28-Oct-11	On-going (c)	1.3	10	0	0
CO94-PZMxxx	BP-MW-10	0.01	na	na	0	0	0	0
CO91-PZMxxx	BP-MW-07	0.08	na	na	0	0	0	0
CO90-PZMxxx	BP-MW-06	0	na	na	0	0	0	0
CO100-PZMxxx	RW-05	0	na	na	0	0	0	0
CO93-PZMxxx	BP-MW-09	0	na	na	0	0	0	0
CO19-PZM004	CO19-PZM004	0	na	na	0	0	0	0
				Total Recovery:	**15,797**	**115,761**	**744**	**5,452**

Notes:

(a) Weight is calculated based on average BP-MW-05 and BP-MW-08 oil density of 0.878 grams per cubic centimeter, measured by EA (2009) by ASTM Method D1481

(b) Skimmer

(c) Bailing

(d) Cumulative recovery volumes are calculated using an estimated recovery from 12/28/11 to 1/18/12 as well as 5/24/12 to 6/22/12.

Table 14
Depths (feet) to Water and LNAPL
Cell 6: LNAPL Recovery System in Former Benzol Processing Area
Former Coke Oven Area Interim Remedial Measures
Sparrows Point, LLC

Date	CO89-PZM			CO90-PZM			CO91-PZM		
	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness
6/30/2016	10.76	11.85	1.09	-	10.06	0	10.62	10.70	0.08

Date	CO92-PZM			CO93-PZM			CO94-PZM		
	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness
6/30/2016	11.81	12.19	0.38	-	10.35	0	7.86	7.87	0.01

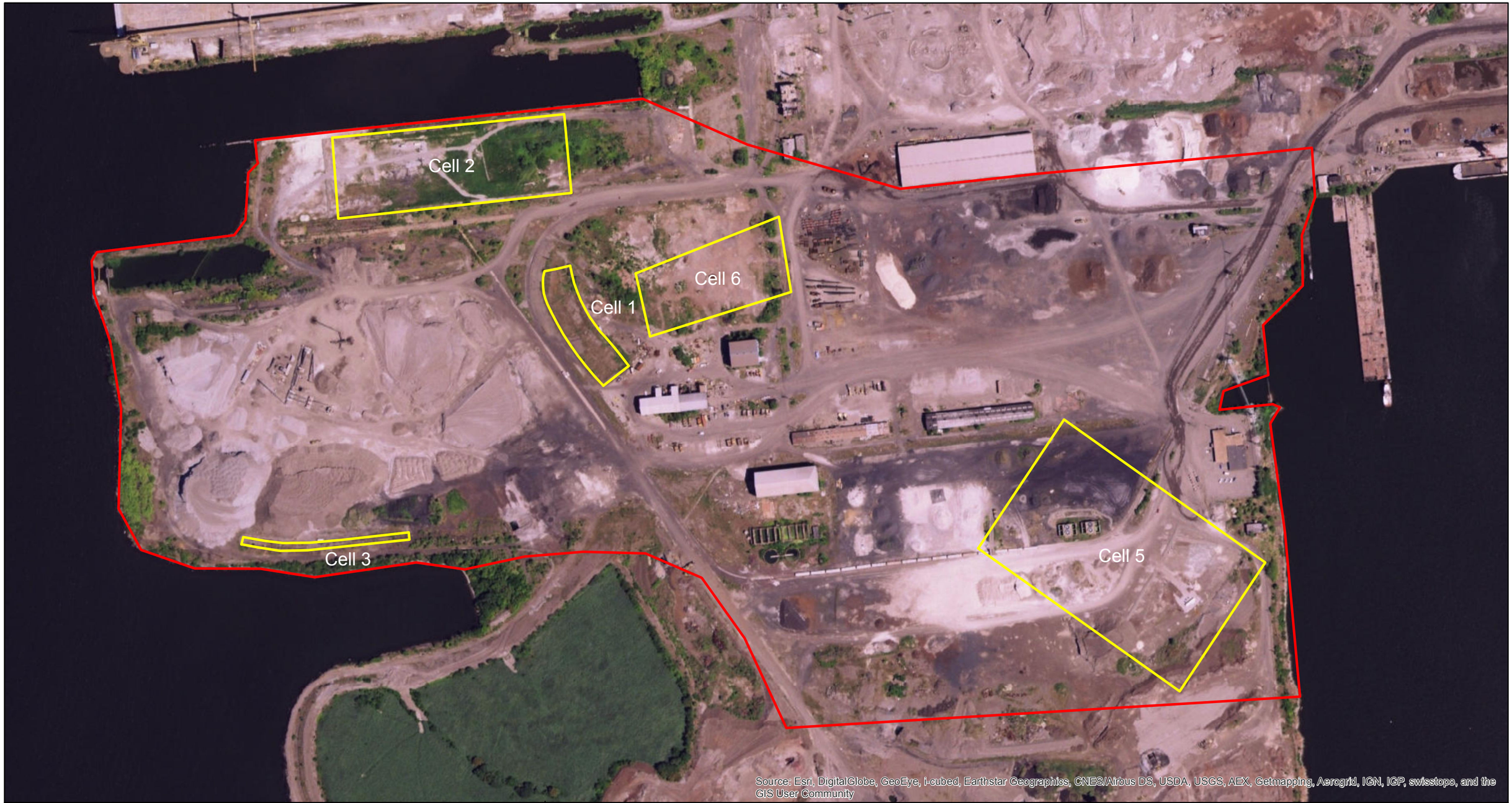
.

Date	CO95-PZM			CO96-PZM			CO97-PZM		
	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness
6/30/2016	12.45	13.47	1.02	11.01	11.20	0.19	9.67	9.71	0.04

Date	CO98-PZM			CO99-PZM			CO100-PZM		
	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness	Depth to LNAPL	Depth to Water	LNAPL Thickness
6/30/2016	8.85	9.04	0.19	9.69	10.06	0.37	-	9.56	0

Date	CO19-PZM004		
	Depth to LNAPL	Depth to Water	LNAPL Thickness
6/30/2016	-	10.28	0

FIGURES



N

EnviroAnalytics Group

Environmental Engineers

1 inch = 350 feet

0 300 600 Feet

Former Coke Oven Area
Interim Measures Cell Locations

Legend

- Former COA IM Cells
- Former Coke Oven Area Boundary

Figure

1

N

EnviroAnalytics Group

Environmental Engineers

1 inch = 88 feet

0 60 120 Feet

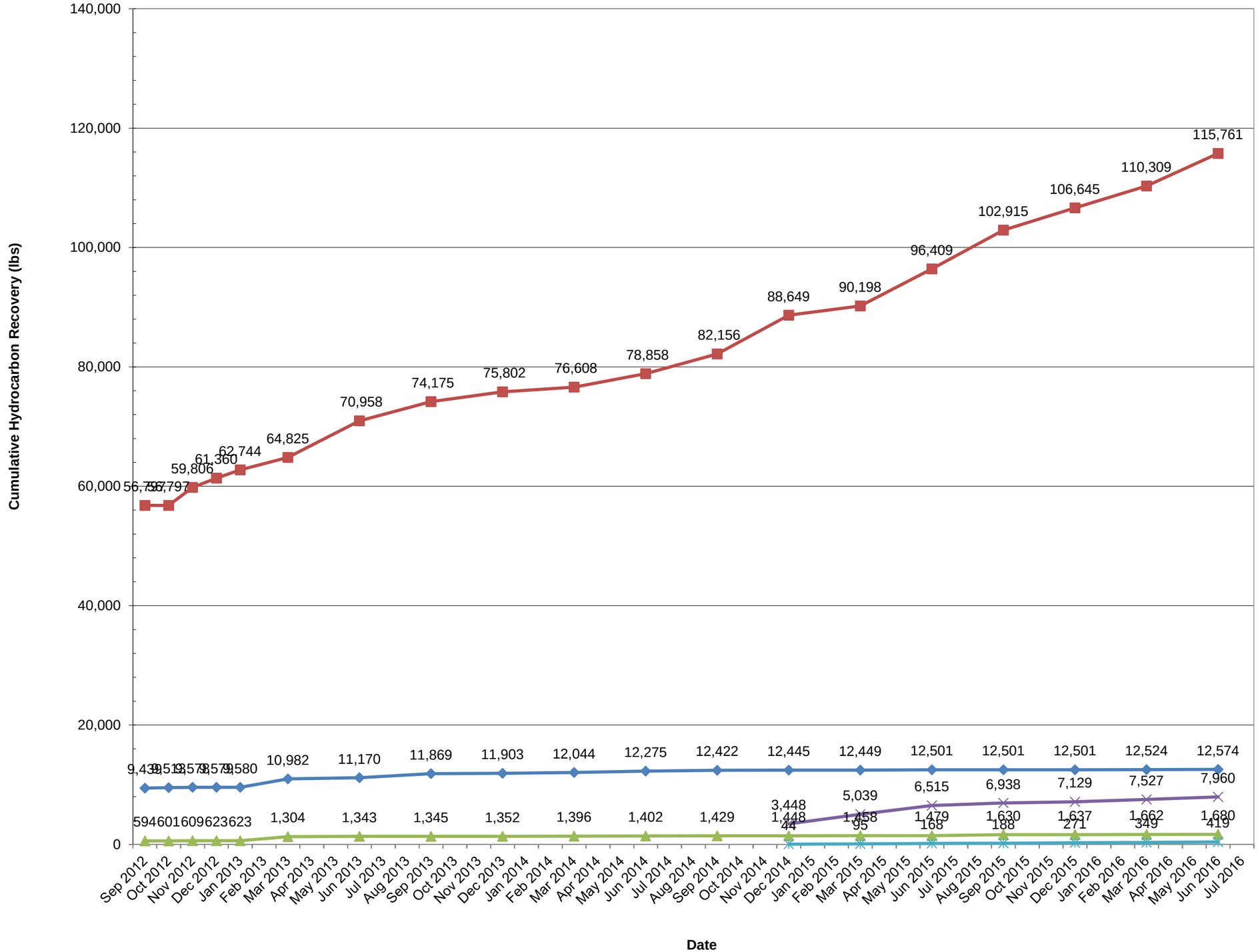
Former Coke Oven Area
Cell 1 AS/SVE System Layout

Legend

- Monitoring Well
- Vapor Extraction Header
- Air Sparge Well
- Vapor Collection Trench

Figure

2



LEGEND

- Cell 1
- Cell 2
- Cell 3
- Cell 5
- Cell 6

EnviroAnalytics Group

Environmental Engineers

Project

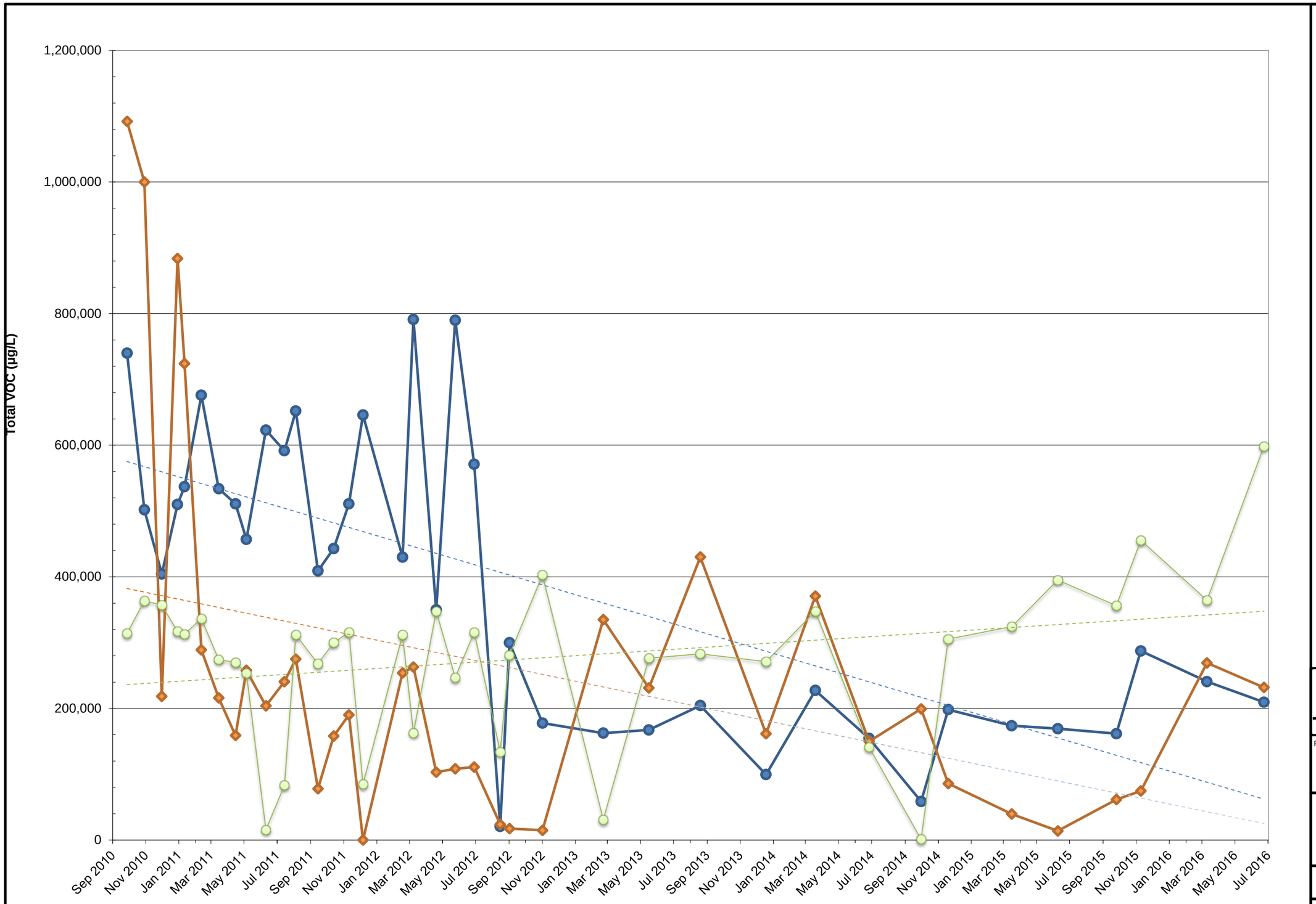
Sparrow Point Terminal, LLC
Baltimore, Maryland

CUMULATIVE SUMMARY OF ESTIMATED HYDROCARBON RECOVERY FORMER COKE OVEN AREA INTERIM REMEDIAL MEASURES

Project Number	File Number

Date	Figure
June 30, 2016	3

PE/RG	PM	DR



LEGEND

- CO02-PZM006
- CO18-PZM006
- CO93-PZMxxx

EnviroAnalytics Group

Environmental Engineers

Project

Tradepoint Atlantic
Baltimore, Maryland

**MEASURED GROUNDWATER VOC CONCENTRATION BY MONTH
CELL 1: PROTOTYPE AS/SVE SYSTEM
IN THE FORMER BENZOL PROCESSING AREA**

Date	Figure
June 30, 2016	4

PE/RG	PM	DR

N

EnviroAnalytics Group

Environmental Engineers

1 inch = 67 feet

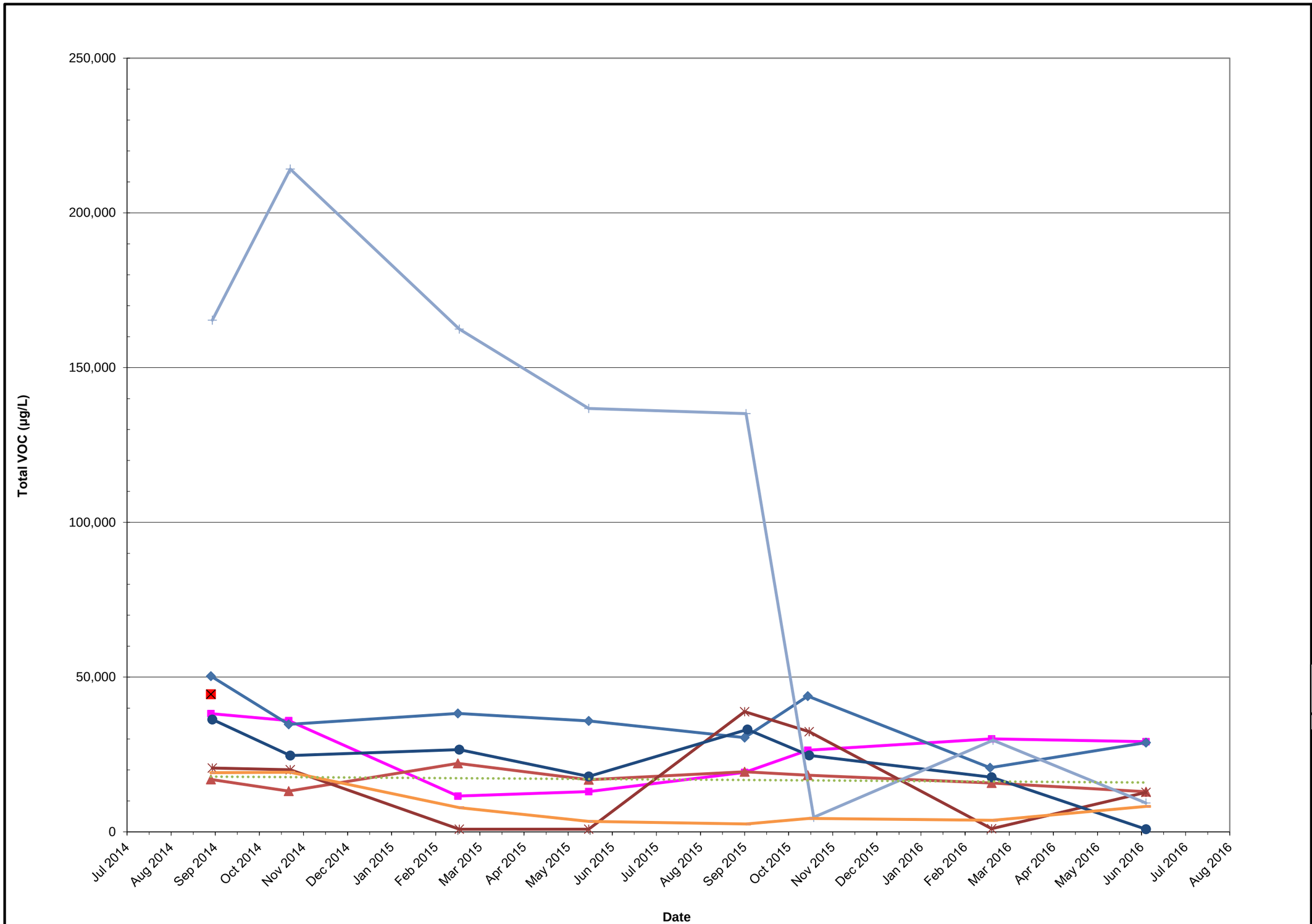
0 50 100 Feet

Former Coke Oven Area Cell 2 System Layout AS/SVE and GW P&T

Legend

- Monitoring Well Shallow Zone
- Monitoring Well Intermediate Zone
- Groundwater Extraction Well
- Reinjection Well
- Air Sparge Well
- Vapor Extraction Header
- Vapor Collection Trench

Figure 5



LEGEND

- CO27-PZM012
- CO36-PZM008
- CO37-PZM003
- CO38-PZM006
- CO39-PZM007
- CO40-PZM008
- CO41-PZM001
- CO42-PZM004
- Linear (CO38-PZM006)

EnviroAnalytics Group

Environmental Engineers

Project

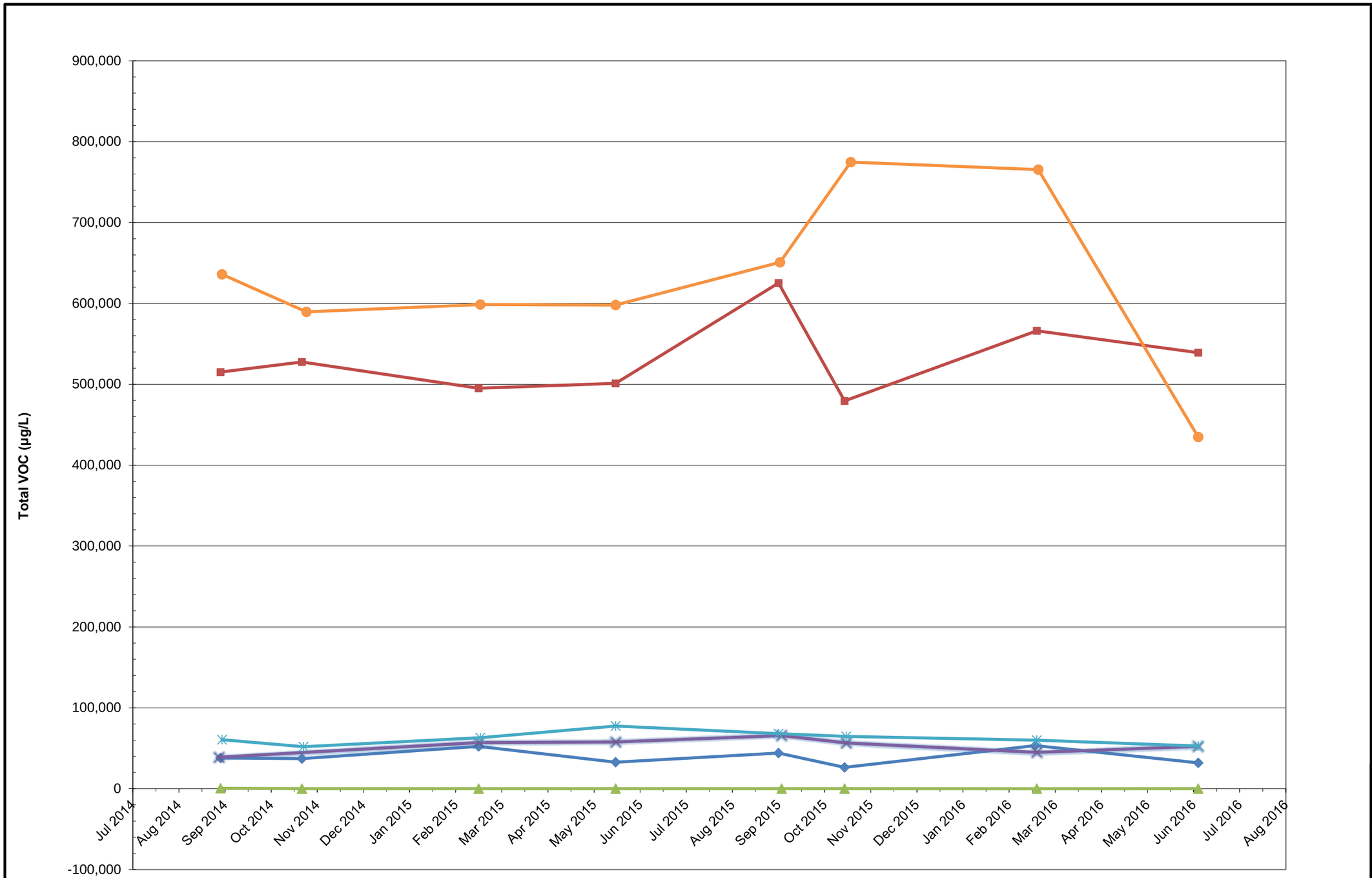
Tradepoint Atlantic
Baltimore, Maryland

MEASURED GROUNDWATER VOC CONCENTRATION BY MONTH
CELL 2: GROUNDWATER PUMP AND TREAT SYSTEM
SHALLOW ZONE

Date: June 30, 2016

Figure: 6A

PE/RG | PM | DR



LEGEND

- CO27-PZM046
- CO36-PZM043
- CO37-PZM038
- CO38-PZM043
- CO39-PZM042
- CO41-PZM036
- Linear (CO38-PZM043)

EnviroAnalytics Group

Environmental Engineers

Project

Tradepoint Atlantic
Baltimore, Maryland

MEASURED GROUNDWATER VOC CONCENTRATION BY MONTH
CELL 2: GROUNDWATER PUMP AND TREAT SYSTEM
INTERMEDIATE ZONE

Date	Figure
June. 30, 2016	6B

PE/RG	PM	DR

N

EnviroAnalytics Group

Environmental Engineers

1 inch = 100 feet

0 75 150 Feet

Former Coke Oven Area
Cell 2 Monitoring Wells Intermediate Zone
Benzene Concentrations Q2 2016

Legend

Monitoring Well Intermediate Zone

Monitoring Wells Sampled 6/22/2016

Figure

7

N

EnviroAnalytics Group

Environmental Engineers

1 inch = 50 feet

0 50 100 Feet

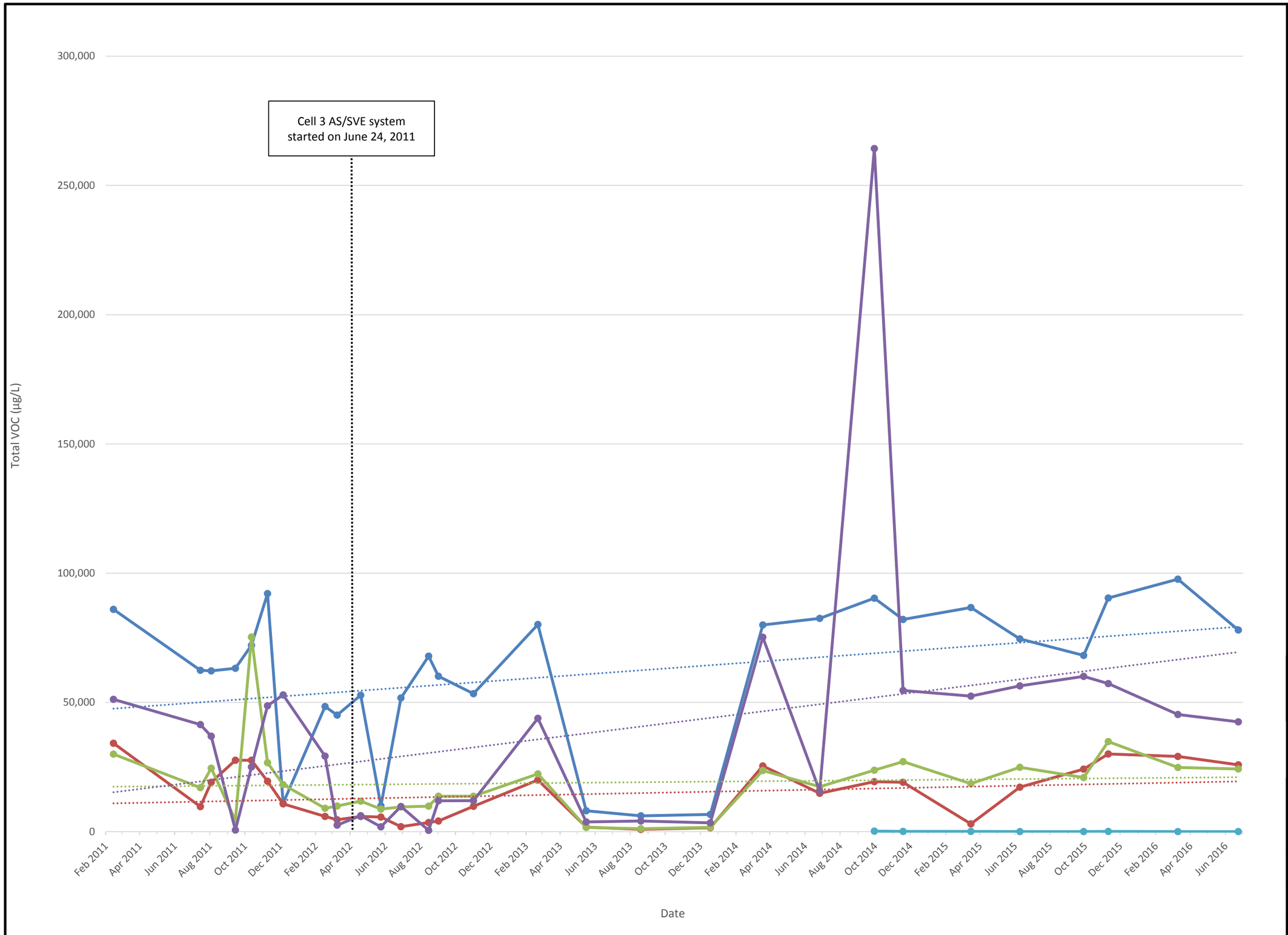
Former Coke Oven Area
Cell 3 AS/SVE System Layout

Legend

- Monitoring Well Shallow Zone
- Air Sparge Well
- Vapor Extraction Header
- Vapor Collection Trench

Figure

8



EnviroAnalytics Group

Environmental Engineers

Project

Tradepoint Atlantic
Baltimore, Maryland

MEASURED GROUNDWATER VOC CONCENTRATION BY MONTH CELL 3: PROTOTYPE AS/SVE SYSTEM IN THE COVE AREA

Date	Figure
June 30, 2016	9

PE/RG	PM	DR

N

EnviroAnalytics Group
Environmental Engineers

1 inch = 133 feet

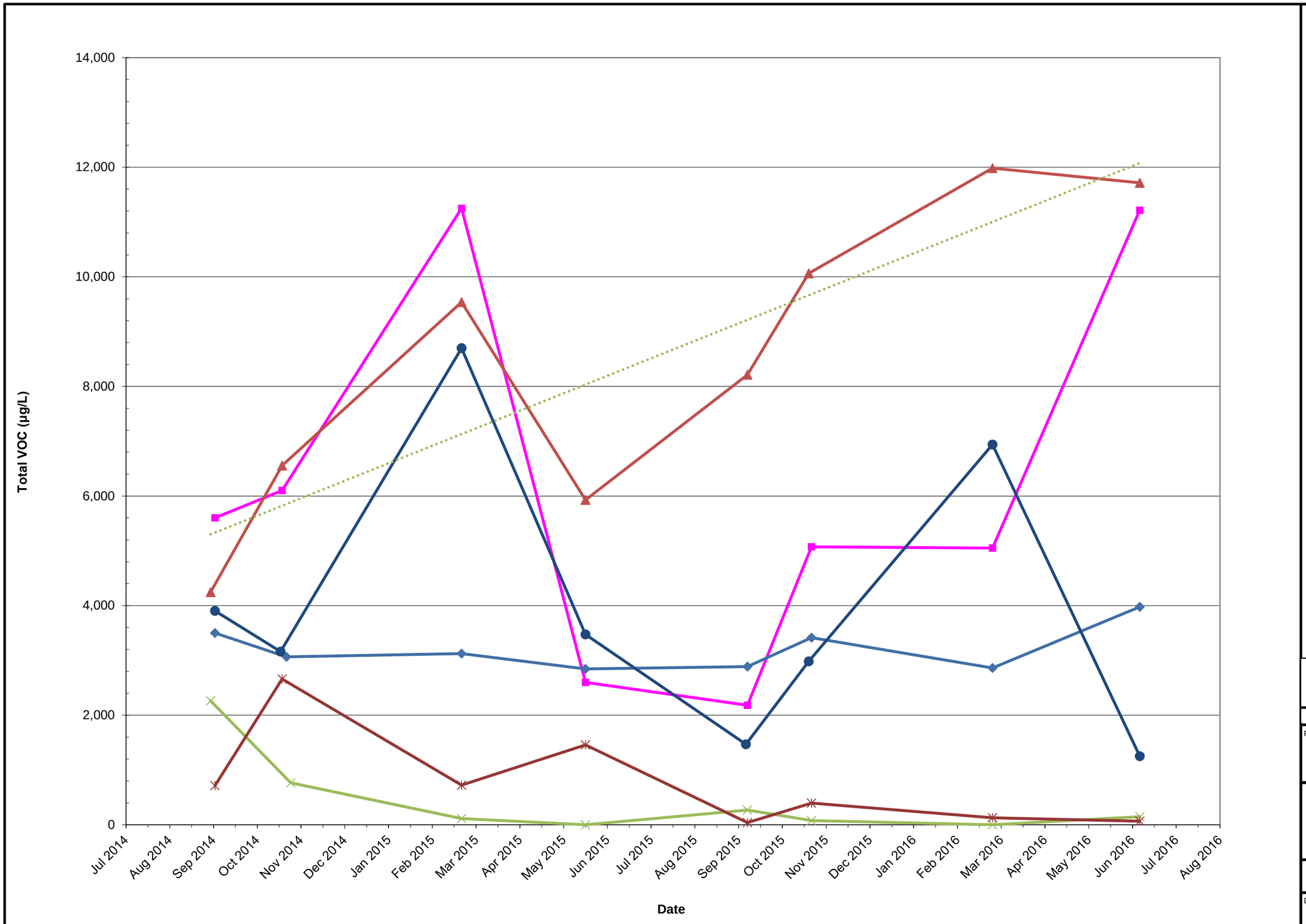
0 125 250 Feet

Former Coke Oven Area
Cell 5 System Layout
DPE System and DNAPL Recovery Pumps

Legend

- Monitoring Well Shallow Zone
- DPE Well
- Reinjection Well
- GW Extraction Area
- DNAPL Recovery Well
- Naphthalene Source Area

Figure 10



EnviroAnalytics Group

Environmental Engineers

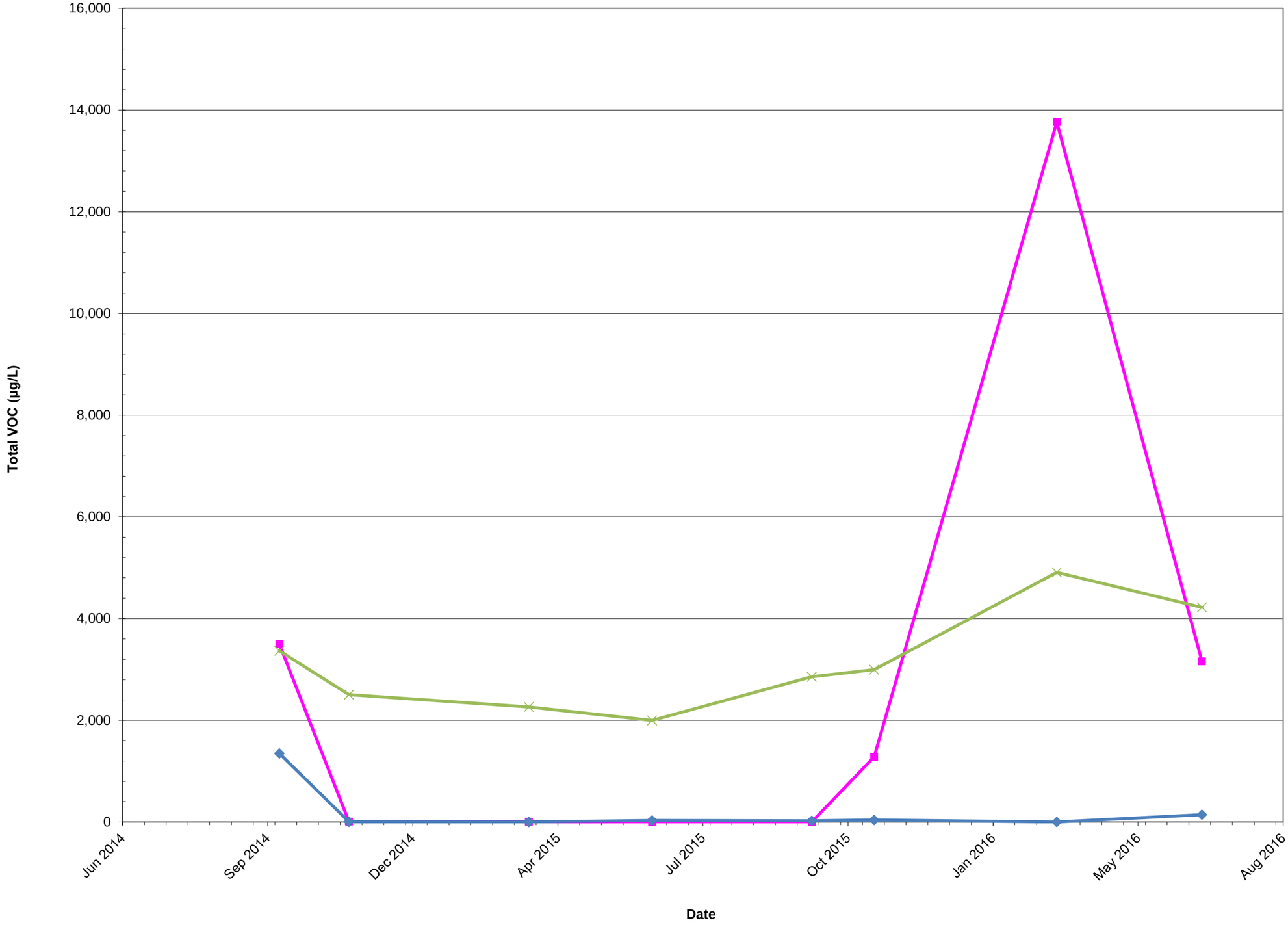
Project

Tradepoint Atlantic
Baltimore, Maryland

**MEASURED GROUNDWATER VOC CONCENTRATION BY MONTH
CELL 5: DPE GROUNDWATER PUMP AND TREAT SYSTEM**

Date	Figure
June 30, 2016	11A

PE/RG	PM	DR



LEGEND

- CO26-PZM007
- CO57-PZP002
- CO58-PZM001

EnviroAnalytics Group

Environmental Engineers

Project

Tradepoint Atlantic
Baltimore, Maryland

**MEASURED GROUNDWATER VOC CONCENTRATION BY MONTH
CELL 5: DPE GROUNDWATER PUMP AND TREAT SYSTEM**

Date	Figure
June 30, 2016	11B

PE/RG	PM	DR

N

EnviroAnalytics Group

Environmental Engineers

1 inch = 150 feet

0 150 300 Feet

Former Coke Oven Area
Cell 5 Monitoring Wells Shallow Zone
Naphthalene Concentrations Q2 2016

Legend

Monitoring Well Shallow Zone

Monitoring Wells Sampled 6/24/2016

Figure

12

N

EnviroAnalytics Group
Environmental Engineers

1 inch = 50 feet

0 50 100 Feet

Former Coke Oven Area
Cell 6 Monitoring Well Locations

Legend

- Monitoring Well Shallow Zone
- LNAPL Source Area

Figure

13